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**(54) Exhaust emission control catalyst**

(57) An exhaust emission control catalyst which is capable of exhibiting an excellent NO<sub>x</sub> converting ability in an excessive-oxygen atmosphere even after being exposed to a high-temperature environment including oxygen and water vapor. The catalyst contains a crystalline aluminosilicate with a catalytic metal carried thereon and CeO<sub>2</sub> as the basic forming components. The crystalline aluminosilicate has at least one of Mg, Ca, Sr, Ba, Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd, Ir, Pb

and Sn carried thereon. The catalytic metal exhibits an oxidizing ability and a reducing ability to an exhaust gas. The crystalline aluminosilicate has a function of adsorbing HC to concentrate it and to supply such HC to the catalytic metal. Each of Mg, Ca, Sr, and Ba has a function of maintaining the function of the crystalline aluminosilicate, and each of the other metal elements has a function of maintaining the function of the catalytic metal.

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## Description

The present invention relates to an exhaust emission control catalyst.

Japanese Patent Application Laid-open No.8-131838 discloses an exhaust emission control catalyst that includes a crystalline aluminosilicate with a catalytic metal carried thereon, namely, a zeolite with Pt carried thereon, and  $\text{CeO}_2$ . The present inventors have made various examinations of that catalyst and, as a result, found that if that catalyst is exposed to a high-temperature environment including oxygen and water vapor, namely, a hydrothermal environment, there is a tendency for it to deteriorate, resulting in a reduced  $\text{NO}_x$  (nitrogen oxides) converting ability in an excessive-oxygen atmosphere.

It is an object of the present invention to provide an exhaust emission control catalyst of the above-described type, wherein the catalyst is further developed and even after it is exposed to a hydrothermal environment as described above, the  $\text{NO}_x$  converting ability can be maintained at a high level.

To achieve the above object, according to the present invention, there is provided an exhaust emission control catalyst comprising, as basic components, a crystalline aluminosilicate with a catalytic metal carried thereon, and  $\text{CeO}_2$ , wherein at least one of Mg, Ca, Sr, Ba, Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd, Ir, Pb and Sn is carried on said crystalline aluminosilicate.

With the above feature, the catalytic metal exhibits an oxidizing ability and a reducing ability to an exhaust gas. The oxidizing ability of the catalytic metal contributes to an oxidizing reaction represented by  $\text{HC}$  (hydrocarbon) +  $\text{O}_2 \rightarrow \text{H}_2\text{O} + \text{CO}_2$  and  $\text{CO} + \text{O}_2 \rightarrow \text{CO}_2$ . The reducing ability of the catalytic metal contributes to a reducing reaction represented by  $\text{NO}_x + \text{CO} \rightarrow \text{N}_2 + \text{CO}_2$  and  $\text{NO}_x + \text{HC} \rightarrow \text{N}_2 + \text{CO}_2 + \text{H}_2\text{O}$  by adsorbing  $\text{NO}_x$  at a theoretically ideal air-fuel ratio (stoichiometric). On the other hand, the reducing ability of the catalytic metal contributes to an oxidizing reaction represented by  $\text{NO}_x + \text{O}_2 \rightarrow \text{NO}_2$  and a reducing reaction represented by  $\text{NO}_2 + \text{HC} + \text{O}_2 \rightarrow \text{H}_2\text{O}$  in the excessive-oxygen atmosphere.

The crystalline aluminosilicate has a function to adsorb HC in an exhaust gas to concentrate it and to supply such HC to the catalytic metal. Thus, it is possible to enhance the  $\text{NO}_x$  conversion rate in the excessive-oxygen atmosphere.

The  $\text{CeO}_2$  exhibits an  $\text{NO}_x$  adsorbing ability in the excessive-oxygen atmosphere and hence, the concentration of  $\text{NO}_x$  in the vicinity of the catalytic metal is increased. This also makes it possible to enhance the  $\text{NO}_x$  conversion rate in the excessive-oxygen atmosphere.

Among the various metal elements, each of Mg, Ca, Sr and Ba has an effect of inhibiting the removal of aluminum from a skeleton structure of the crystalline aluminosilicate in a hydrothermal environment as described above. Thus, the heat resistance of the crystalline aluminosilicate is enhanced, and even after the catalyst is exposed to the hydrothermal environment, the crystalline aluminosilicate can satisfactorily exhibit the above-described function in the excessive-oxygen atmosphere.

Each of Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd and Ir has an effect of inhibiting the growth of catalytic metals due to the sintering of them in the hydrothermal environment. Thus, the dispersability of the catalytic metal can be maintained even after the catalyst is exposed to the hydrothermal environment.

Further, each of Pb and Sn has an effect of permitting oxygen adsorbed on the catalytic metal to overflow toward Pb, Sn or the like, namely, generating a spill-over phenomenon. Thus, the adsorption of HC, CO,  $\text{NO}_x$  and the like to the catalytic metal is promoted in a range of low temperature of an exhaust gas and hence, it is possible to enhance the ability to oxidize HC and CO at a low temperature and to enhance the ability to convert  $\text{NO}_x$  produced in the SCR (selective catalytic reduction). The same is true even after exposure of the catalyst to the hydrothermal environment.

In addition, according to the present invention, there is provided an exhaust emission control catalyst comprising, as basic forming components, a crystalline aluminosilicate with a catalytic metal carried thereon, and  $\text{CeO}_2$ , wherein at least one of La and Ba is included in said  $\text{CeO}_2$ . The  $\text{CeO}_2$  including La and/or Ba has a high  $\text{NO}_x$  adsorbing ability in an excessive-oxygen atmosphere compared with the  $\text{CeO}_2$  not including La or the like and hence, it is possible to further enhance the  $\text{NO}_x$  converting ability in such atmosphere. The same is true even after exposure of the catalyst to the hydrothermal environment.

## BRIEF DESCRIPTION OF THE DRAWINGS:

Fig. 1 is an illustration for explaining  $\text{CeO}_2$ .

Fig. 2 is a graph illustrating the relationship between the proportion  $c_1$  of Mg by weight and the maximum NO conversion rate.

Fig. 3 is a graph illustrating a first example of the relationship between the catalysts as examples of this invention and comparative examples, and the maximum NO conversion rate.

Fig. 4 is a graph illustrating a second example of the relationship between the catalysts as examples of this invention and comparative examples, and the maximum NO conversion rate.

Fig. 5 is a graph illustrating a third example of the relationship between the catalysts as examples of this invention

and comparative examples, and the maximum NO conversion rate.

Fig. 6 is a graph illustrating a fourth example of the relationship between the catalysts as examples of this invention and comparative examples, and the maximum NO conversion rate.

A first embodiment of an exhaust emission control catalyst of this invention includes a crystalline aluminosilicate having a catalytic metal carried thereon and  $\text{CeO}_2$  as basic components. Platinum is used as the catalytic metal, and zeolite is used as the crystalline aluminosilicate.

At least one of the following metals is carried as a metal element Me on the zeolite: Mg, Ca, Sr, Ba, Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd, Ir, Pb, and Sn.

The zeolite may be an MFI-type zeolite having a relatively good heat-resistance, e.g., a ZSM-5 zeolite. This ZSM-5 zeolite may be an unmodified one, but if heat resistance to a high-temperature exhaust gas during operation of an engine is considered, it is desirable to use a modified ZSM-5 zeolite produced by subjecting the unmodified zeolite to a de-aluminization.

The de-aluminization of the unmodified ZSM-5 zeolite which may be utilized is at least one of an acid treatment, a steaming treatment, and a boiled-water treatment.

The acid treatment may be a process which involves heating an HCl solution of 0.5 to 5 N to a temperature in a range of 70 to 90°C, placing the unmodified ZSM-5 zeolite in such HCl solution and agitating the solution containing the unmodified ZSM-5 zeolite for 1 to 20 hours.

The boiled-water treatment may be a process which involves subjecting the unmodified ZSM-5 zeolite to a hydrating treatment, rising the atmospheric temperature around the hydrated unmodified ZSM-5 zeolite to 550 to 600°C, and maintaining the unmodified ZSM-5 zeolite under such high-temperature atmosphere for 4 hours.

The steaming treatment may be a process which involves maintaining the unmodified ZSM-5 zeolite in an atmosphere including water of about 10 % and having a temperature in a range of 750 to 900°C for 10 to 20 hours.

The acid treatment, the boiled-water treatment and the steaming treatment may be utilized alone or in combination of two or more of them, and may be repeated, if required. In this manner, a modified ZSM-5 zeolite is produced and has a  $\text{SiO}_2/\text{Al}_2\text{O}_3$  molar ratio in a range of 25 to 800.

In such a modified ZSM-5 zeolite, the crystallizability is enhanced by the de-aluminizing treatment, and the generation of the nucleus of a pyrolysis product is inhibited. Therefore, the heat-resistant temperature of the modified ZSM-5 zeolite is increased to about 100°C.

A ZSM-5 zeolite having Pt carried thereon is produced by allowing platinum (Pt) to be carried on a modified ZSM-5 zeolite by an ion exchanging process, an impregnating process or the like.

Platinum (Pt) which is a catalytic metal exhibits an oxidizing ability and a reducing ability to an exhaust gas.

The oxidizing ability of platinum contributes to an oxidizing reaction represented by  $\text{HC (hydrocarbon)} + \text{O}_2 \rightarrow \text{H}_2\text{O} + \text{O}_2$  and  $\text{CO} + \text{O}_2 \rightarrow \text{CO}_2$ .

The reducing ability of platinum contributes to a reducing reaction represented by  $\text{NO} + \text{CO} \rightarrow \text{N}_2 + \text{CO}_2$  and  $\text{NO} + \text{HC} \rightarrow \text{N}_2 + \text{H}_2\text{O} + \text{CO}_2$  which is caused by adsorption of  $\text{NO}_x$ , e.g., NO in this embodiment at a theoretical air-fuel ratio, on the one hand, and contributes to an oxidizing reaction represented by  $\text{NO} + \text{O}_2 \rightarrow \text{NO}_2$  and a reducing reaction represented by  $\text{NO}_2 + \text{HC} + \text{O}_2 \rightarrow \text{N}_2 + \text{CO}_2 + \text{H}_2\text{O}$  at an excessive-oxygen atmosphere, on the other hand.

The modified ZSM-5 zeolite has a hydrophobic nature enhanced by the de-aluminizing treatment and a basic skeleton structure possessed by the unmodified ZSM-5 zeolite, and moreover, has a specific surface area enlarged by the removal of aluminum. Therefore, the adsorbing ability which is a characteristic of the modified ZSM-5 zeolite is promoted. Such modified ZSM-5 zeolite exhibits a good adsorbing ability to HC in an exhaust gas even in the presence of water to concentrate HC and also exhibits a function to supply the HC to platinum. Thus, it is possible to enhance the rate of purification of NO in the excessive-oxygen atmosphere.

$\text{CeO}_2$  exhibits an NO adsorbing ability in the excessive-oxygen atmosphere and hence, the concentration of NO in the vicinity of platinum (Pt). This also makes it possible to enhance the rate of purification of NO in the excessive-oxygen atmosphere.

$\text{CeO}_2$  is formed of polycrystalline grains each of which is comprised of a plurality of crystallites congregated, as shown in Fig. 1. To cause the  $\text{CeO}_2$  to exhibit the above-described function, the average diameter D of the crystallites is set in a range of  $D < 500\text{\AA}$ , preferably, in a range of  $D \leq 320\text{\AA}$ .

In producing  $\text{CeO}_2$ , any of various Ce salts such as Ce carbonate, Ce oxalate, Ce nitrate and the like is heated in the presence of oxygen. When pure  $\text{CeO}_2$  free from any rare earth element is produced,  $\text{CeO}_2$  produced after heating is washed with nitric acid.

The control of the average diameter D of the crystallites is performed by regulating the heating temperature in the producing course. For example, for  $\text{CeO}_2$  having an average diameter D of crystallites equal to 78Å, Ce nitrate is heated at about 250°C for 5 hours. The average diameter D of the crystallites can be also controlled by subjecting the produced  $\text{CeO}_2$  to a thermal treatment. For example, if the  $\text{CeO}_2$  having the average diameter of 78Å is subjected to the thermal treatment at 700°C for 30 hours,  $\text{CeO}_2$  having an average diameter D of 205Å is produced.

To calculate a diameter  $D_{(hkl)}$  of crystallites, the Schuler equation, i.e.,  $D_{(hkl)} = 0.9\lambda/(\beta_{1/2} \cdot \cos\theta)$  was used, wherein

$hkl$  is Miller index;  $\lambda$  is a wavelength ( $\text{\AA}$ ) of characteristic X-rays;  $\beta_{1/2}$  is a half-value width (radian) of a ( $hkl$ ) face; and  $\theta$  is an X-ray reflection angle. Therefore, in the  $\text{CeO}_2$ , a diameter  $D_{(111)}$  of each of the crystallites was calculated by measuring the half-value width  $\beta_{1/2}$  of a (111) face from an X-ray diffraction pattern, and an average diameter  $D$  of the crystallites was determined from the diameters  $D_{(111)}$  of the crystallites:

Each of the various metal elements Me is carried on a modified ZSM-5 zeolite having platinum carried thereon or having no platinum carried thereon by an impregnating process or an ion exchanging process. Each of Mg, Ca, Sr and Ba as the metal elements Me has an effect of inhibiting the removal of aluminum from the skeleton structure of the modified ZSM-5 zeolite in a hydrothermal environment as described above. Thus, it is possible to enhance the heat resistance of the modified ZSM-5 zeolite, thereby causing the modified ZSM-5 zeolite to sufficiently exhibit the above-described function in the excessive-oxygen atmosphere even after being exposed to the hydrothermal environment.

Each of Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd and Ir has an effect of inhibiting the growth due to the sintering of Pt molecules in the hydrothermal environment. Thus, it is possible to maintain the dispersability of Pt even after being exposed to the hydrothermal environment.

Further, each of Pb and Sn has an effect of allowing oxygen adsorbed on Pt to overflow toward Pb or Sn, namely for generating a spill-over phenomenon. Thus, the adsorption of HC, CO, NO and the like to Pt is promoted in a range of low temperature of the exhaust gas and hence, it is possible to enhance the ability to oxidize HC and CO at a low temperature and to enhance the ability to convert NO produced in SCR in such lower-temperature range. This is also true even after exposure to the hydrothermal environment.

If the weight of Pt-Me carried modified ZSM-5 zeolite with Pt and a metal element Me carried thereon, which is incorporated in the catalyst, is represented by  $A$ , and the weight of  $\text{CeO}_2$  incorporated in the catalyst is represented by  $B$ , the proportion  $A_1 = \{A/(A+B)\} \times 100$  of the Pt-Me carried modified ZSM-5 zeolite by weight is set in a range of 19 % by weight  $< A_1 < 100$  % by weight. If the weight of Pt-carried modified ZSM-5 zeolite incorporated is represented by  $a$ , and the weight of Pt is represented by  $b$ , the proportion  $b_1 = (b/a) \times 100$  of Pt by weight is set in a range of 3.5 % by weight  $\leq b_1 \leq 11$  % by weight. Further, if the proportion of Pt-Me carried modified ZSM-5 zeolite incorporated is represented by  $A$ , and the weight of metal element Me incorporated is represented by  $c$ , the proportion  $c_1 = (c/A) \times 100$  of the metal element by weight is set in a range of a minimum effective amount of the metal element to  $c_1 \leq 10$  % by weight. The upper limit value of this proportion  $c_1$  is varied in principle depending upon the type of the metal element Me in the range of  $c_1 \leq 10$  % by weight.

However, if the proportion  $A_1$  of the Pt-Me carried modified ZSM-5 zeolite by weight is in a range of  $A_1 \leq 19$  % by weight, the HC absorbing ability of the Pt-Me carried modified ZSM-5 zeolite is reduced and for this reason, the NO conversion rate is decreased. On the other hand, if  $A_1 = 100$  %, the ability to adsorb NO by  $\text{CeO}_2$  is not obtained and hence, the NO conversion rate is decreased. If the proportion  $b_1$  of Pt by weight is lower than 3.5 % by weight, the amount of Pt carried is smaller and hence, the NO conversion rate is decreased. On the other hand, even if the proportion  $b_1$  of Pt by weight is set in a range of  $b_1 > 11$  % by weight, the NO conversion rate is varied only a little. Further, if the proportion  $c_1$  of the metal element Me by weight is larger than 10 % by weight, pores in the surface of the ZSM-5 zeolite are occluded by the metal element Me, whereby the function of the zeolite is reduced, resulting in a decreased NO conversion rate of the catalyst.

A second embodiment of an exhaust emission control catalyst of this invention includes a crystalline aluminosilicate having a catalytic metal carried thereon and  $\text{CeO}_2$  as basic components, as in the first embodiment. Pt is used as the catalytic metal, as in the first embodiment, and a zeolite such as a modified ZSM-5 zeolite is used as the crystalline aluminosilicate, as in the first embodiment. At least one of La and Ba is contained in the  $\text{CeO}_2$  in this second embodiment.

The  $\text{CeO}_2$  including La and/or Ba as described above has a high NO adsorbing ability in an excessive-oxygen atmosphere, as compared with  $\text{CeO}_2$  including no La or Ba and hence, the NO conversion rate in such atmosphere can be further enhanced. This is also true even after exposure to the hydrothermal environment.

The production of the Pt-carried modified ZSM-5 zeolite and  $\text{CeO}_2$  is carried out in the same manner as in the first embodiment.

In producing the  $\text{CeO}_2$  including La and/or Ba, namely, La-including  $\text{CeO}_2$ , Ba-including  $\text{CeO}_2$  and La-Ba-including  $\text{CeO}_2$ , lanthanum nitrate is used as La, and barium nitrate is used as Ba. The steps of suspending  $\text{CeO}_2$  into a solution of each of the lanthanum nitrate and the barium nitrate, agitating, drying and calcining the suspension are conducted in sequence.

If the weight of Pt-carried modified ZSM-5 zeolite incorporated in the catalyst is represented by  $E$ , and the weight of La-including  $\text{CeO}_2$ , Ba-including  $\text{CeO}_2$  or La-Ba-including  $\text{CeO}_2$  incorporated in the catalyst is represented by  $F$ , the proportion  $E_1 = \{E/(E+F)\} \times 100$  of the Pt-carried modified ZSM-5 zeolite is set in a range of 19 % by weight  $< E_1 < 100$  % by weight. If the weight of Pt-carried modified ZSM-5 zeolite incorporated is represented by  $a$ , and the weight of Pt incorporated is represented by  $b$ , the proportion  $b_1 = (b/a) \times 100$  of Pt by weight is set in a range of 3.5 % by weight  $\leq b_1 \leq 11$  % by weight. Further, if the weight of La-including  $\text{CeO}_2$ , Ba-including  $\text{CeO}_2$  or La-Ba-including  $\text{CeO}_2$  incorporated is represented by  $d$ , and the weight of La, Ba or La + Ba incorporated is represented by  $e$ , the proportion

$e_1 \{= (e/d) \times 100\}$  of La, Ba or both by weight is set in a range of 5 % by weight  $\leq e_1 \leq 25$  % by weight.

However, if the proportion  $E_1$  of the Pt-carried modified ZSM-5 zeolite is equal to or smaller than 19 % by weight, the HC adsorbing ability of the Pt-carried modified ZSM-5 zeolite is reduced and for this reason, the NO conversion rate is decreased. On the other hand, if the proportion  $E_1$  is equal to 100 %, the ability to adsorb NO by the La-including  $\text{CeO}_2$  or the like is not obtained and hence, the NO conversion rate is decreased. If the proportion  $b_1$  of Pt is smaller than 3.5 % by weight, the amount of Pt carried is smaller and hence, the NO conversion rate is decreased. On the other hand, if the proportion  $b_1$  of Pt is set in a range of  $b_1 > 11$  % by weight, the NO conversion rate is varied only a little. Further, if the proportion  $e_1$  of La or the like is smaller than 5 % by weight, there is no effect created by the fact that some La or the like is contained. On the other hand, if  $e_1$  is  $> 25$  % by weight, the amount of La-including  $\text{CeO}_2$  is decreased and hence, the NO conversion is decreased, and the contribution to the purification is decreased, as compared with the case where the  $\text{CeO}_2$  is contained along in the catalyst.

Various examples of the invention and comparative examples, as well as the processes used in making and testing them will now be described. First, the production of the modified ZSM-5 zeolite used in all the examples will be described.

#### Production of modified ZSM-5 zeolite:

1. An unmodified ZSM-5 zeolite having a  $\text{SiO}_2/\text{Al}_2\text{O}_3$  molar ratio of 42 was placed in a 5N solution of HCl at  $90^\circ\text{C}$ , and the resulting solution was agitated for 20 hours to provide a slurry-like matter.
2. Solids were separated from the slurry-like matter by filtering and washed with pure water, until the pH of the washing water reached a value equal to or larger than 4.
3. The solids were subjected to a drying treatment under conditions of  $130^\circ\text{C}$  for 5 hours and then to a calcining treatment at  $400^\circ\text{C}$  for 12 hours in the atmosphere, thereby providing a massive modified ZSM-5 zeolite.
4. The massive modified ZSM-5 zeolite was subjected to a pulverizing treatment to provide a powdery modified ZSM-5 zeolite. The  $\text{SiO}_2/\text{Al}_2\text{O}_3$  molar ratio of this powdery modified ZSM-5 zeolite was 54 and hence, it can be seen that the de-aluminization occurred. The heat-resistant temperature of the powdery modified ZSM-5 zeolite was  $1,000^\circ\text{C}$ .

#### Example A:

In this example A, a catalyst will be described which contains, as a component, a Pt-Me carried modified ZSM-5 zeolite using Mg as the metal element Me.

#### A. De-aluminization inhibiting effect of Mg

Magnesium (Mg) was carried on the modified ZSM-5 zeolite under utilization of an ion exchanging process as described below, thereby providing a Me-carried modified ZSM-5 zeolite.

- (a) An aqueous solution of 6-hydrated magnesium nitrate  $[\text{Mg}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}]$  having a predetermined concentration was added in an amount of 400ml to the modified ZSM-5 zeolite of a predetermined incorporated weight to provide a mixture.
- (b) Using an evaporator, water was removed from the mixture, thereby providing an Mg-carried modified ZSM-5 zeolite by the impregnating process.
- (c) The Mg-carried modified ZSM-5 zeolite was subjected to a drying under conditions of  $120^\circ\text{C}$  and 3 hours in the atmosphere and then to a calcining treatment at  $400^\circ\text{C}$  for 12 hours in the atmosphere.

Table 1 shows the weight of incorporation of the modified ZSM-5 zeolite (corresponding to ZSM-5 shown in the Table) used in the production in examples 1 and 2 of the Mg-carried modified ZSM-5 zeolite, the concentration of the 6-hydrated magnesium nitrate (corresponding to  $\text{Mg}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  shown in the Table) in the aqueous solution, and the proportion of Mg in the examples 1 and 2.

Table 1

Mg-carried modified ZSM-5 zeolite		Weight of ZSM-5 incorporated (g)	Concentration of Mg $(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ (g/liter)	Proportion of Mg (% by weight)
Example	1	49.7	6.7	0.51
	2	49.5	13.5	1.05

Then, the examples 1 and 2 of the Mg-carried modified ZSM-5 zeolite and the modified ZSM-5 zeolite without Mg as a comparative example were subjected to MAS27Al-NMR measurement, thereby determining the proportion of Al within the skeleton. The measuring conditions were as follows: the standard sample was an aqueous solution of 1 mole of aluminum chloride; the number of rotations of the sample was 6,000 rpm; the frequency of addition was 200; the moderating time was 5 seconds; the spectrum treating conditions were T3 = 20, T4 = 40 and BF = 100.

Then, the examples 1 and 2 and the comparative example were subjected to an aging treatment in which they were maintained for 20 hours in a gas atmosphere consisting of 10 % by weight of O<sub>2</sub>, 10 % by weight of H<sub>2</sub>O and the balance of N<sub>2</sub> at a temperature of 700°C, namely, they were exposed to a hydrothermal environment. Thereafter, the proportion of Al within the skeleton of each of the examples 1 and 2 and the comparative example was determined in the same manner as described above.

Table 2 shows the proportion of Mg in the examples 1 and 2 and the comparative example, the proportions G and H of Al within the skeleton before and after the aging treatment, and the de-aluminization rate K [= {(G - H) / G} x 100].

Table 2

Mg-carried modified ZSM-5 zeolite		Proportion of Mg (% by weight)	Proportion of Al within the skeleton (% by weight)		de-aluminization rate K (%)
			G before aging treatment	H after aging treatment	
Example	1	0.51	93.0	81.8	12.0
	2	1.05	96.0	86.4	10.0
Comparative Example		-	95.1	47.9	49.6

As apparent from Table 2, the de-aluminization rates K of the examples 1 and 2 are remarkably lower than that of the comparative example. This is presumed to be due to the fact that magnesium entered pores in the examples 1 and 2 and acted with ion exchange sites which are Brönsted acid sites within the pores in the zeolite, i.e., with aluminum within the skeleton, thereby stabilizing the charge balance between Me-Al and the zeolite, and hence, the removal of aluminum was inhibited.

#### B. Production of Pt-Mg carried modified ZSM-5 zeolite

- 25 grams of platinum dinitrodiamine was dissolved in 1,000 ml of 25 % ammonia water by heating to provide a platinum solution (having a Pt concentration of 1.5 %).
- 100 grams of the modified ZSM-5 zeolite was added to the platinum solution, and the resulting mixture was agitated at 90°C for 12 hours to cause Pt to be carried on the modified ZSM-5 zeolite by the ion exchange process.
- After cooling, the Pt-carried modified ZSM-5 zeolite was separated by filtering and then washed with pure water.
- The Pt-carried modified ZSM-5 zeolite was subjected to a drying treatment at 120°C for 3 hours in the atmosphere and then to a calcining treatment at 400°C for 12 hours in the atmosphere. The proportion b<sub>1</sub> of Pt in the Pt-carried modified ZSM-5 zeolite was equal to 7.6 % by weight.
- Magnesium was carried on the Pt-carried modified ZSM-5 zeolite by an impregnating process which will be described below, thereby providing a Pt-Mg-carried ZSM-5 zeolite.

(a) An aqueous solution of 6-hydrated magnesium nitrate [Mg(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O] having a predetermined concentration was added in an amount of 400 ml to the Pt-carried modified ZSM-5 zeolite having a predetermined incorporation weight to provide a mixture.

(b) An evaporator was used to remove water from the mixture.

(c) The mixture was subjected to a drying treatment at 120°C for 3 hours in the atmosphere and then to a calcining treatment at 400°C for 12 hours in the atmosphere.

Table 3 shows the weight of incorporation of the Pt-carried modified ZSM-5 zeolite used for the production of examples 1 to 5 of the Pt-Mg-carried modified ZSM-5 zeolite (corresponding to PtZSM-5 shown in Table 3), the concentration of the 6-hydrated magnesium nitrate (corresponding to Mg(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O shown in Table 3) in the aqueous solution, and proportion c<sub>1</sub> of Mg in the examples 1 to 5.



Table 3

Pt-Mg-carried modified ZSM-5 zeolite		Weight of PtZSM-5 incorporated (g)	Concentration of Mg (NO <sub>3</sub> ) <sub>2</sub> ·6H <sub>2</sub> O (g/liter)	Proportion c <sub>1</sub> of Mg (% by weight)
Examples	1	50.0	1.33	0.10
	2	49.8	6.60	0.52
	3	49.7	13.30	1.00
	4	50.0	20.15	1.50
	5	49.0	26.38	1.95

In addition, as another example, magnesium was carried on the Pt-carried modified ZSM-5 zeolite by utilizing an ion exchange process which will be described below, thereby providing a Pt-Mg-carried modified ZSM-5 zeolite.

(a) An aqueous solution of 6-hydrated magnesium nitrate [Mg(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O] having a predetermined concentration was added in an amount of 400 ml to the Pt-carried modified ZSM-5 zeolite having a predetermined incorporation weight, and they were mixed together. Then, 25 % ammonia water was added to the mixture, so that the pH of the mixture was regulated to 8. Thereafter, the mixture was heated to 90°C and agitated for 12 hours. Thus, a Pt-Mg-carried modified ZSM-5 zeolite was produced by the ion exchange process.

(b) After cooling, the Pt-Mg-carried modified ZSM-5 zeolite was separated by filtering and then washed with pure water.

(c) The Pt-Mg-carried modified ZSM-5 zeolite was subjected to a drying treatment at 120°C for 3 hours in the atmosphere and then to a calcining treatment at 400°C for 12 hours in the atmosphere.

Table 4 shows the weight of incorporation of the Pt-carried modified ZSM-5 zeolite used for the production of examples 6 to 8 of the Pt-Mg-carried modified ZSM-5 zeolite (corresponding to PtZSM-5 shown in Table 4), the concentration of the 6-hydrated magnesium nitrate (corresponding to Mg(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O shown in Table 4) in the aqueous solution, and proportion c<sub>1</sub> of Mg in the examples 6 to 8.

Table 4

Pt-Mg-carried modified ZSM-5 zeolite		Weight of PtZSM-5 incorporated (g)	Concentration of Mg (NO <sub>3</sub> ) <sub>2</sub> ·6H <sub>2</sub> O (g/liter)	Proportion c <sub>1</sub> of Mg (% by weight)
Examples	6	50.0	123.3	0.16
	7	50.0	246.6	0.18
	8	49.8	246.6	0.42

#### C. Aging Treatment

The examples 1 to 8 of the Pt-Mg carried modified ZSM-5 zeolite were subjected to an aging treatment under the same conditions.

#### D. Production of catalyst

30 grams of the above-described example 1 of the Pt-Mg carried modified ZSM-5 zeolite resulting from the aging treatment, 60 grams of CeO<sub>2</sub> having an average diameter D of 78Å, 50 grams of 20 % silica sol, 180 grams of pure water and alumina balls were thrown into a pot, and they were subjected to a wet pulverization for 12 hours to prepare a slurry-like catalyst. In this case, the composition of the catalyst comprises 30 % by weight of the Pt-Mg carried modified ZSM-5 zeolite, 60 % by weight of CeO<sub>2</sub> and 10 % by weight of SiO<sub>2</sub>. Therefore, the proportion A<sub>1</sub> of the Pt-Mg carried modified ZSM-5 zeolite is nearly equal to 33 % by weight (A<sub>1</sub> ≈ 33 % by weight). On the other hand, the proportion B<sub>1</sub> [= {B/(A + B)} × 100] of the CeO<sub>2</sub> is nearly equal to 67 % by weight.

A 6 mil honeycomb support made of cordierite having a diameter of 25.5 mm, a length of 60 mm and 400 cells/in<sup>2</sup> was immersed into the slurry-like catalyst. Then, the honeycomb support was taken out from the slurry-like catalyst, and an excessive amount of the catalyst was removed by jetting of air. Thereafter, the honeycomb support was maintained under heating at 150°C for 1 hour to dry the slurry-like support and further it was subjected to a calcining

treatment at 400°C for 12 hours in the atmosphere, thereby supporting the catalyst on the honeycomb support. In this case, the amount of catalyst retained on the honeycomb support was 150 g/liter. This catalyst is referred to as catalyst example 1.

Using the examples 2 to 8 of the above-described Pt-Mg carried modified ZSM-5 zeolite, catalyst examples 2 to 8 were produced in the same manner as described above.

For comparison, using a Pt-carried modified ZSM-5 zeolite resulting from an aging treatment similar to that described above in place of the Pt-Mg-carried modified ZSM-5 zeolite, a comparative example of catalyst was produced in the same manner as described above. The proportion of the Pt-carried modified ZSM-5 zeolite in this comparative example was about 33 % by weight, and the proportion of CeO<sub>3</sub> was about 67 % by weight.

#### E. Test of purification of supposed exhaust gas

A test gas having a composition shown in Table 5 was prepared as a simulation gas in a case of an air-fuel ratio A/F = 24 that simulates the exhaust gas during a low-load lean burn.

Table 5

Component	Test gas A/F = 24 (% by volume)
CO <sub>2</sub>	1.0
H <sub>2</sub>	0.03
C <sub>3</sub> H <sub>6</sub>	0.12
NO	0.02
CO	0.1
O <sub>2</sub>	10.0
H <sub>2</sub> O	10.0
N <sub>2</sub>	balance

In the purifying test, the catalyst of the example 1 was first placed in a fixed-bed flow reaction device. Then, the test gas was allowed to flow through the device at a space velocity S.V. of  $5 \times 10^4 \text{ h}^{-1}$ , and at the same time, the temperature of the test gas was risen at a rising rate of 20°C/min to 500°C. The NO conversion rate by the catalyst of the example 1 during this time was measured. A similar purifying test was also carried out for the catalysts of the examples 2 to 8 and the comparative example.

Table 6 shows the proportion  $c_1$  of Mg and the maximum NO conversion rate with regard to the catalysts of the examples 1 to 8 and the comparative example. In this case, the maximum NO conversion rate of each catalyst is provided at near a gas temperature of 250°C. For example, for the example 6, the gas temperature was 265°C, and for the comparative example, the gas temperature was 240°C.

Table 6

Catalyst	Proportion $c_1$ of Mg (% by weight)	Maximum NO conversion rate (%)
Example	1	0.10
	2	0.52
	3	1.00
	4	1.50
	5	1.95
	6	0.16
	7	0.18
	8	0.42
Comparative example		

Fig.2 is a graph produced from the relationship between the proportion  $c_1$  of Mg and the maximum NO conversion



rate based on Table 6. In Fig.2, points (1) to (8) correspond to the examples 1 to 8, respectively.

As is apparent from Fig.2, if magnesium is carried on the Pt-carried modified ZSM zeolite as in examples 1 to 8, the maximum NO conversion rate can be enhanced in the excessive-oxygen atmosphere even after the aging treatment, more than that in the comparative example. The proportion  $c_1$  of Mg in the catalyst is preferably in a range of  $c_1 \leq 1.5$  % by weight.

#### Example B:

In this example B, a catalyst will be described which includes, as a forming component, a Pt-Me-carried modified ZSM-5 zeolite, wherein Ca, Sr or Ba is used as the metal element Me.

#### A. Production of Pt-Me carried modified ZSM-5 zeolite

##### 1. Carrying of Me

(a) An aqueous solution of Me nitrate having a predetermined concentration was added in an amount of 400 ml to and mixed with 50 grams of the modified ZSM-5 zeolite. Then, the mixture was heated to 90°C and agitated for 12 hours. Thus, a Me-carried modified ZSM-5 zeolite was produced by the ion exchange process.

(b) After cooling, the Me-carried modified ZSM-5 zeolite was separated by filtering and then washed with pure water.

(c) The Me-carried modified ZSM-5 zeolite was subjected to a drying treatment at 120°C for 3 hours in the atmosphere and then to a calcining treatment at 400°C for 12 hours in the atmosphere.

##### 2. Carrying of Pt

(a) 12.5 grams of platinum dinitrodiamine was dissolved into 500 ml of 25 % ammonia water by heating to provide a platinum solution. (having a Pt concentration of 1.5 %).

(b) 50 grams of the Me-carried modified ZSM-5 zeolite was added to the platinum solution, and the mixture was agitated at 90°C for 12 hours. Thus, Pt was carried on the Me-carried modified ZSM-5 zeolite by the ion exchange process.

(c) After cooling, the Pt-Me-carried modified ZSM-5 zeolite was separated by filtering and then washed with pure water.

(d) The Pt-Me-carried modified ZSM-5 zeolite was subjected to a drying treatment at 120°C for 3 hours in the atmosphere and then to a calcining treatment at 400°C for 12 hours in the atmosphere.

Table 7 shows the type of nitrate used for carrying of the Me, the concentration of the nitrate in the aqueous solution, and the proportion  $c_1$  of Me by weight for examples 1 to 3 of the Pt-Me-carried modified ZSM-5 zeolite. The proportion  $b_1$  of Pt in each of the examples 1 to 3 is nearly equal to 7.6 % by weight, as in Example A.

Table 7

Pt-Me-carried modified ZSM-5		Nitrate		Proportion $c_1$ of Me
		Type	Concentration (g/liter)	
Example	1	$\text{Ca}(\text{NO}_3)_2 \cdot 4\text{H}_2\text{O}$	227.1	Ca:0.20
	2	$\text{Sr}(\text{NO}_3)_2 \cdot 4\text{H}_2\text{O}$	203.5	Sr:0.51
	3	$\text{Ba}(\text{NO}_3)_2 \cdot 4\text{H}_2\text{O}$	125.7	Ba:0.51

B. Each of the examples 1 to 3 of the Pt-Me-carried modified ZSM-5 zeolite was subjected to an aging treatment under the same condition as those described above.

C. Using examples 1 to 3 of Pt-Me-carried modified ZSM-5 zeolite resulting from the aging treatment, examples 1 to 3 of catalyst were produced in the same process as that described in section D in Example A.

Then, the catalysts of the examples 1 to 3 were subjected to a purifying test in a method similar to that described in the section E in Example A.

Table 8 shows the type of metal element Me, the maximum NO conversion rate and the gas temperature at the

time when the maximum NO conversion rate was obtained for the examples 1 to 3 and, as a comparative example, the catalyst shown in Table 6.

Table 8

Catalyst		Type of metal element Me	Maximum NO conversion rate (%)	Gas temperature (°C)
Example	1	Ca	48.2	262
	2	Sr	47.9	258
	3	Ba	54.5	250
Comparative example		-	41.3	240

Fig 3 is a graph produced from the relationship between the catalysts of the examples 1 to 3 and the comparative example and the maximum NO conversion rate, based on Table 8.

As is apparent from Fig.3, if Ca, Sr or Ba is carried on the Pt-carried modified ZSM-5 zeolite as in examples 1 to 3 the maximum NO conversion rate can be enhanced in the excessive-oxygen atmosphere even after the aging treatment more than that with the catalyst as the comparative example. This is attributable to the fact that the removal of aluminum from the modified ZSM-5 zeolite was inhibited by Ca, Sr and Ba, as in the case where Mg was carried.

#### Example C

In this example C, a catalyst will be described which includes, as a forming component, a Pt-Me-carried modified ZSM-5 zeolite wherein Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd or Ir is used as the metal element Me.

A. An Me-carried modified ZSM-5 zeolite was produced in a process similar to that described in the item 1 of section A in Example B, except that the type of the metal salt and the concentration of the metal salt in the aqueous solution were varied.

Then a Pt-Me-carried modified ZSM-5 zeolite was produced in a method similar to that described in the item 2 of section A in Example B.

Table 9 shows the type of metal salt used for carrying of the Me, the concentration of the metal salt in the aqueous solution and the proportion  $c_1$  of Me by weight, for the examples 1 to 13 of the Pt-Me-carried modified ZSM-5 zeolite. The proportion  $b_1$  of Pt in each of the examples 1 to 13 is nearly equal to 7.6 % by weight, as in Example A.

Table 9

Pt Me carried modified ZSM-5 zeolite		Metal salt		Proportion $c_1$ of Me (% by weight)
		Type	Concentration (g/liter)	
Example	1	TiCl <sub>4</sub>	182.4	Ti:3.00
	2	VOC <sub>2</sub> O	62.5	V:0.16
	3	Fe(NO <sub>3</sub> ) <sub>3</sub> ·9H <sub>2</sub> O	388.6	Fe:0.43
	4	Zn(CH <sub>3</sub> COO) <sub>2</sub>	211.1	Zn:7.80
	5	Ga(NO <sub>3</sub> ) <sub>3</sub> ·8H <sub>2</sub> O	50.0	Ga:0.20
	6	YCl <sub>3</sub>	136.8	Y:0.16
	7	ZrO(NO <sub>3</sub> ) <sub>2</sub>	257.0	Zr:1.60
	8	MoCl <sub>5</sub>	125.0	Mo:0.50
	9	InCl <sub>3</sub>	125.0	In:0.74
	10	La(NO <sub>3</sub> ) <sub>3</sub> ·6H <sub>2</sub> O	416.5	La:0.44
	11	Ce(NO <sub>3</sub> ) <sub>3</sub> ·6H <sub>2</sub> O	417.6	Ce:0.07
	12	Nd(NO <sub>3</sub> ) <sub>3</sub> ·6H <sub>2</sub> O	210.8	Nd:0.09
	13	IrCl <sub>3</sub>	31.3	Ir:1.30

B. The examples 1 to 13 of the Pt-Me-carried modified zeolite were subjected to an aging treatment under the

same conditions as those described above.

C. Using examples 1 to 13 of Pt-Me-carried modified zeolite resulting from the aging treatment, examples 1 to 13 of catalyst were produced in a process similar to that described in the section D in Example A.

Then, the examples 1 to 13 were subjected to a purifying test in a method similar to that described in the section E in Example A. Table 10 shows the type of the metal element Me, the maximum NO conversion rate and the gas temperature at the time when such maximum NO conversion rate was obtained, for the examples 1 to 13 and, as the comparative example, the catalyst shown in Table 6.

Table 10

Catalyst		Type of metal element Me	Maximum NO conversion rate (%)	Gas temperature (°C)
Example	1	Ti	45.0	250
	2	V	48.5	245
	3	Fe	48.8	260
	4	Zn	46.8	255
	5	Ga	47.5	260
	6	Y	51.1	250
	7	Zr	44.5	252
	8	Mo	50.9	250
	9	In	51.4	255
	10	La	50.8	260
	11	Ce	49.2	250
	12	Nd	48.4	260
	13	Ir	44.8	258
Comparative example		-	41.3	240

Fig 4 is a graph produced from the relationship between catalysts as the examples 1 to 13 and the comparative example and the maximum NO conversion rate based on Table 10.

As is apparent from Fig.4, if Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd or Ir is carried on the Pt-carried modified ZSM-5 zeolite as in the catalysts of the examples 1 to 13, the maximum NO conversion rate can be enhanced in the excessive-oxygen environment even after the aging treatment, more than that with the catalyst as the comparative example. This is attributable to a Pt-growth inhibiting effect provided by each of the metal elements of examples 1 to 13.

#### Example D:

In this Example D, a catalyst will be described which includes, as a forming component, a Pt-Me-carried modified ZSM-5 zeolite wherein Pb or Sn was used as the metal element Me.

A. An Me-carried modified ZSM-5 zeolite was produced in a process similar to the process described in the item 1 of section A in Example B, except that the type of metal salt and the concentration of the metal salt in the aqueous solution were varied.

Then, a Pt-Me-carried modified ZSM-5 zeolite was produced in a process similar to that described in the item 2 of section A in Example B.

Table 11 shows the type of metal salt used for carrying the Me, the concentration of the metal salt in the aqueous solution, and the proportion  $c_1$  of the for the examples 1 and 2 of the Pt-Me-carried modified ZSM-5 zeolite. The proportion  $b_1$  of Pt in each of the examples 1 and 2 is nearly equal to 7.6 % by weight as in Example A.

Table 11

Pt-Me-carried		Metal salt		Proportion $c_1$ of
		Type	Concentration	
Example	1	Pb(CH <sub>3</sub> COO) <sub>2</sub>	364.8	7.90

Table 11 (continued)

Pt-Me-carried		Metal salt		Proportion $c_1$ of
		Type	Concentration	
	2	$\text{SnCl}_4$	319.8	9.60

B. The examples 1 and 2 of the Pt-Me-carried ZSM-5 zeolite were subjected to an aging treatment under the same conditions as those described above.

C. Using examples 1 and 2 of Pt-Me-carried ZSM-5 zeolite resulting from the aging treatment, examples 1 and 2 of catalysts were produced in a process similar to that described in section D in Example A.

Then, The catalysts as the examples 1 and 2 were subjected to a purifying test similar to that described in section E in Example A.

Table 12 shows the type of metal element Me, the maximum NO conversion rate and the gas temperature at the time when such maximum NO conversion rate was obtained, for the catalysts as the examples 1 and 2 and the comparative example shown in Table 6.

Table 12

Catalyst		Type of metal element Me	Maximum NO conversion rate (%)	Gas temperature ( $^{\circ}\text{C}$ )
Example	1	Pb	77.8	210
	2	Sn	54.5	250
Comparative example		-	41.3	240

Fig.5 is a graph taken from the relationship between catalysts as the examples 1 and 2 and the comparative example and the maximum NO conversion rate based on Table 12.

As is apparent from Fig.5, if Pb or Sn is carried on the Pt-carried modified ZSM-5 zeolite as in the catalysts of the examples 1 and 2, the maximum NO conversion rate can be substantially enhanced in the excessive-oxygen environment even after the aging treatment, more than that with the catalyst as the comparative example with no Pb or Sn carried thereon. This is attributable to a spill-over phenomenon generated by Pb and Sn.

#### Example E:

In this Example E, a catalyst will be described which is comprised of a Pt-carried modified ZSM-5 zeolite and  $\text{CeO}_2$  including La or Ba.

#### A. Production of $\text{CeO}_2$ including La or Ba

##### 1. La-including $\text{CeO}_2$

(a) 31.2 grams of 6-hydrated lanthanum nitrate [ $\text{La}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ ] was dissolved in 600 ml of pure water to prepare an aqueous solution.

(b) 90.0 grams of  $\text{CeO}_2$  (having an average diameter D of crystallites equal to 78Å) was suspended in the aqueous solution to provide a La-including  $\text{CeO}_2$  mixture.

(c) Using an evaporator, water was removed from the mixture.

(d) The La-including  $\text{CeO}_2$  mixture was subjected to a drying treatment at 120°C for 3 hours in the atmosphere and then to a calcining treatment at 600°C for 1 hour in the atmosphere. The proportion  $e_1$  of La in the La-including  $\text{CeO}_2$  was equal to 10 % by weight.

##### 2. Ba-including $\text{CeO}_2$

(a) 19.0 gram of barium nitrate [ $\text{Ba}(\text{NO}_3)_2$ ] was dissolved into 600 ml of pure water to prepare an aqueous solution.

(b) 90.0 gram of  $\text{CeO}_2$  (having an average diameter D of crystallites equal to 78) was suspended in the aqueous solution to provide a Ba-including  $\text{CeO}_2$  mixture.

(c) Using an evaporator, water was removed from the mixture.

(d) The Ba-including  $\text{CeO}_2$  mixture was subjected to a drying treatment at 120°C for 3 hours in the atmos-

phere and then to a calcining treatment at 600°C for 1 hours in the atmosphere. The proportion  $e_1$  of Ba in the Ba-including  $\text{CeO}_2$  was equal to 10 % by weight.

B. Using a Pt-carried modified ZSM-5 zeolite (proportion  $b_1$  of Pt = 7.6 % by weight) resulting from the aging treatment and a La-including  $\text{CeO}_2$  or Ba-including  $\text{CeO}_2$ , examples 1 and 2 of catalysts were produced in a process similar to that described in the section D in Example A. In the examples 1 and 2, the proportion  $E_1$  of the Pt-carried modified ZSM-5 zeolite was nearly equal to 33 % by weight, while the proportions  $F_1$  [ $= \{F/(E + F)\} \times 100$ ] of the La-including  $\text{CeO}_2$  and the Ba-including  $\text{CeO}_2$  were nearly equal to 67 % by weight, respectively.

Then, a purifying test was carried out for the catalysts of the examples 1 and 2 in a method similar to that described in the section in Example A.

Table 13 shows the type of  $\text{CeO}_2$ , the maximum NO conversion rate and the gas temperature at the time when such maximum NO conversion rate was obtained, for the catalysts as the examples 1 and 2 and the comparative example shown in Table 6.

Table 13

Catalyst		Type of $\text{CeO}_2$	Maximum NO conversion rate (%)	Gas temperature (°C)
Example	1	La-including $\text{CeO}_2$	43.7	260
	2	Ba-including $\text{CeO}_2$	48.5	270
Comparative example		$\text{CeO}_2$	41.3	240

Fig.6 is a graph produced from the relationship between catalysts as the examples 1 and 2 and the comparative example and the maximum NO conversion rate, based on Table 13.

As is apparent from Fig.6, if La or Ba is carried on the  $\text{CeO}_2$  as in the catalysts of the examples 1 and 2, the maximum NO conversion rate can be enhanced in the excessive-oxygen environment even after the aging treatment, more than that with the catalyst as the comparative example with no La or Ba carried thereon. This is attributable to an NO-adsorbing ability enhancing effect provided by the La-including or Ba-including  $\text{CeO}_2$ .

According to the present invention, it is possible to provide an exhaust emission control catalyst which is capable of exhibiting an excellent  $\text{NO}_x$  converting ability in an excessive-oxygen atmosphere even after being exposed to a high-temperature environment including oxygen and water vapor by the above-described configuration of the catalyst.

## Claims

1. An exhaust emission control catalyst comprising a crystalline aluminosilicate with a catalytic metal carried thereon, and  $\text{CeO}_2$ , wherein either, at least one of Mg, Ca, Sr, Ba, Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd, Ir, Pb and Sn is carried on said crystalline aluminosilicate, or at least one of La and Ba is included in said  $\text{CeO}_2$ .
2. An exhaust emission control catalyst as claimed in claim 1, wherein the proportion by weight of said crystalline aluminosilicate with a catalytic metal carried thereon and at least one of said Mg, Ca, Sr, Ba, Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd, Ir, Pb and Sn to the total weight of the catalyst is in the range of 19% to 100%.
3. An exhaust emission control catalyst as claimed in claim 1, wherein the proportion by weight of at least one of said Mg, Ca, Sr, Ba, Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd, Ir, Pb and Sn to said crystalline aluminosilicate with a catalytic metal carried thereon is less than or equal to 10%.
4. An exhaust emission control catalyst as claimed in claim 1, wherein the proportion by weight of said crystalline aluminosilicate with a catalytic metal carried thereon and said  $\text{CeO}_2$  containing at least one of La and Ba to the total weight of catalyst is in a range of 19% to 100%.
5. An exhaust emission control catalyst as claimed in claim 1 wherein the proportion by weight of at least one of said La and Ba to  $\text{CeO}_2$  and at least one of said La and Ba is in the range 5% to 25%.
6. An exhaust emission control catalyst as claimed in any of the preceding claims wherein the catalytic metal is platinum.

7. An exhaust emission control catalyst comprising, a crystalline aluminosilicate with a catalytic metal carried thereon, and  $\text{CeO}_2$ , wherein a non-catalytic metal element is carried on said crystalline aluminosilicate, said non-catalytic metal element being present in an amount that is effective for inhibiting the removal of aluminium from said crystalline aluminosilicate in a hydrothermal environment.

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8. An exhaust emission control catalyst as claimed in claim 7, wherein said non-catalytic metal element is at least one of Mg, Ca, Sr, Ba, Ti, V, Fe, Zn, Ga, Y, Zr, Mo, In, La, Ce, Nd, Ir, Pb and Sn.

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FIG.1

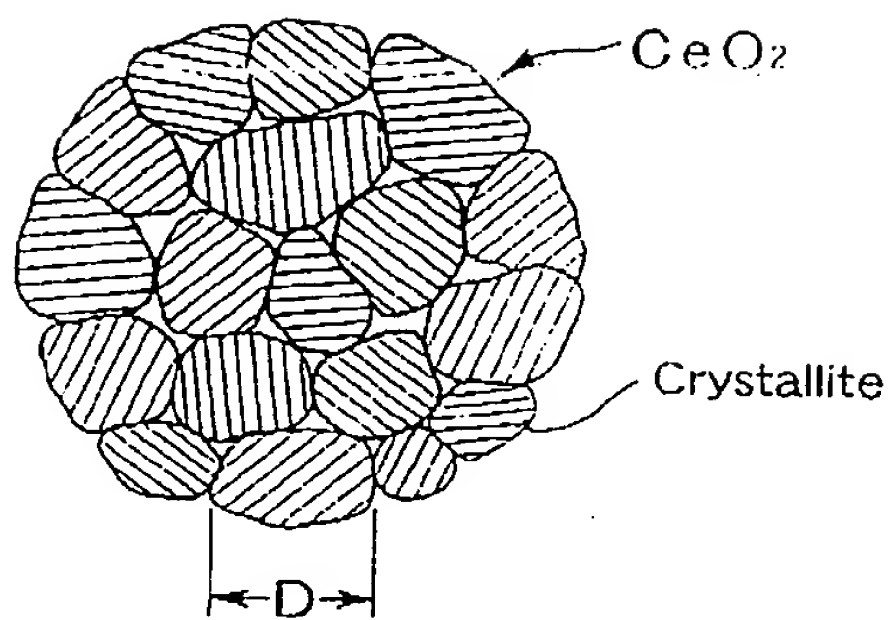


FIG.2

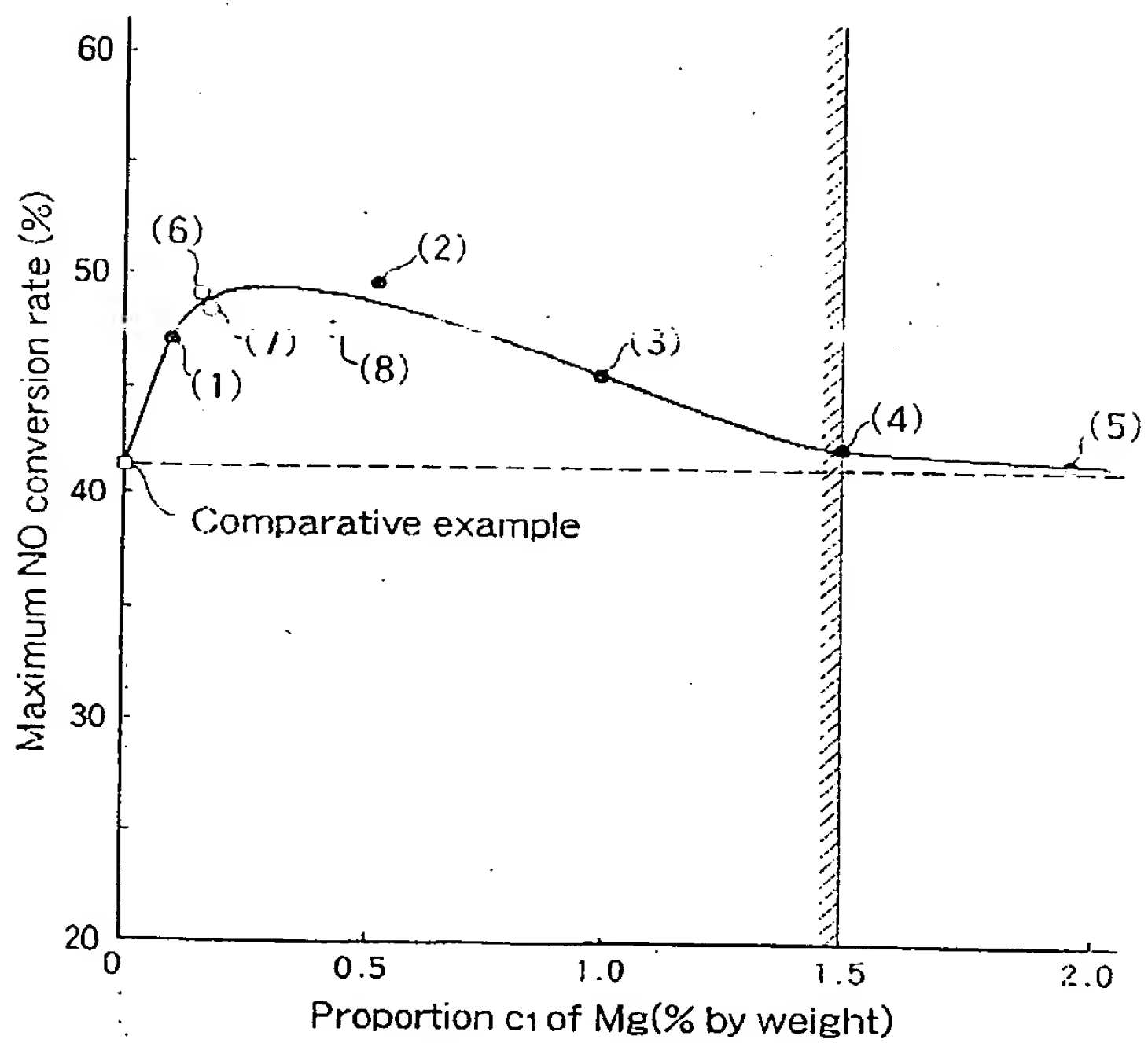


FIG.3

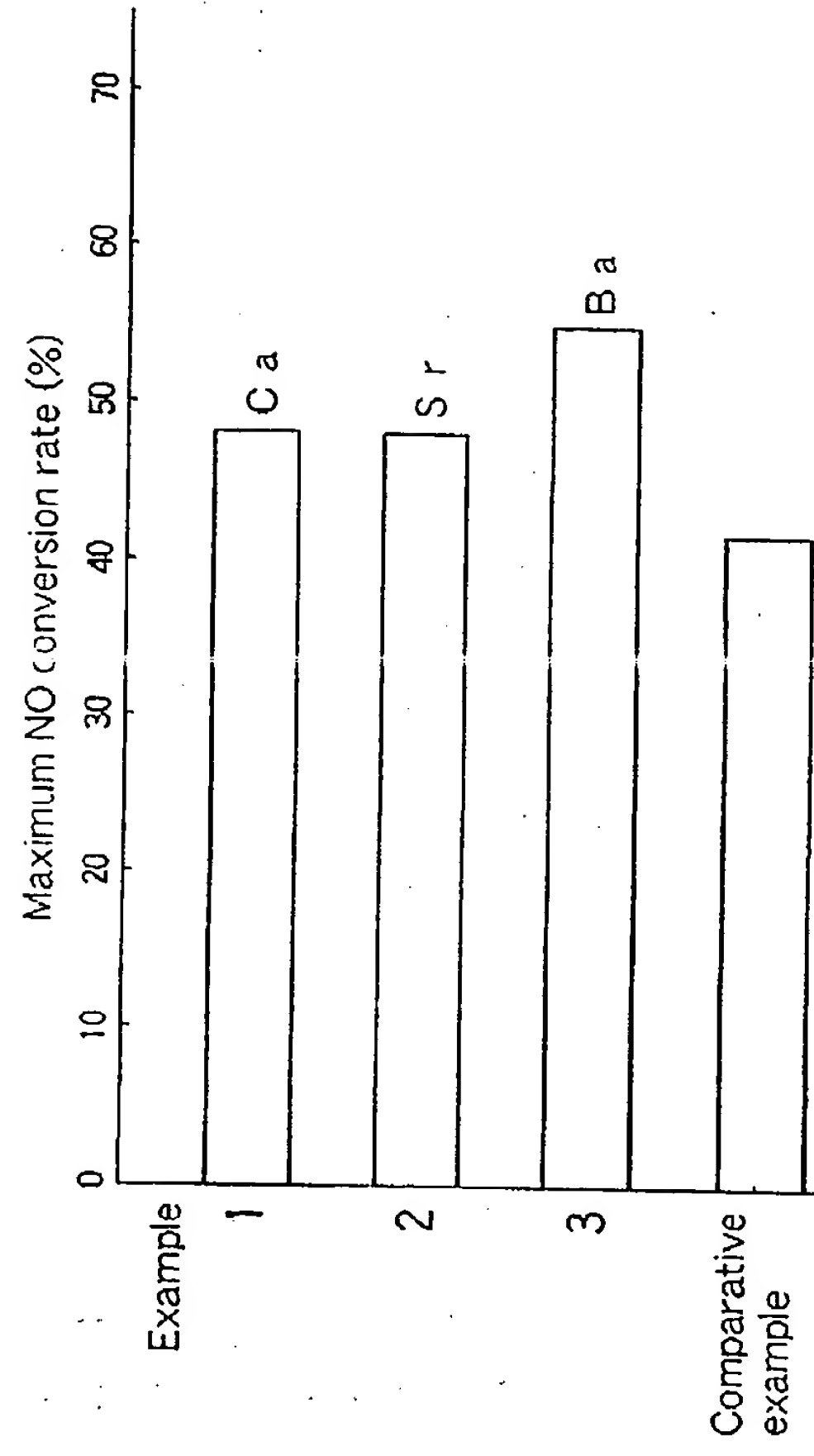


FIG.4

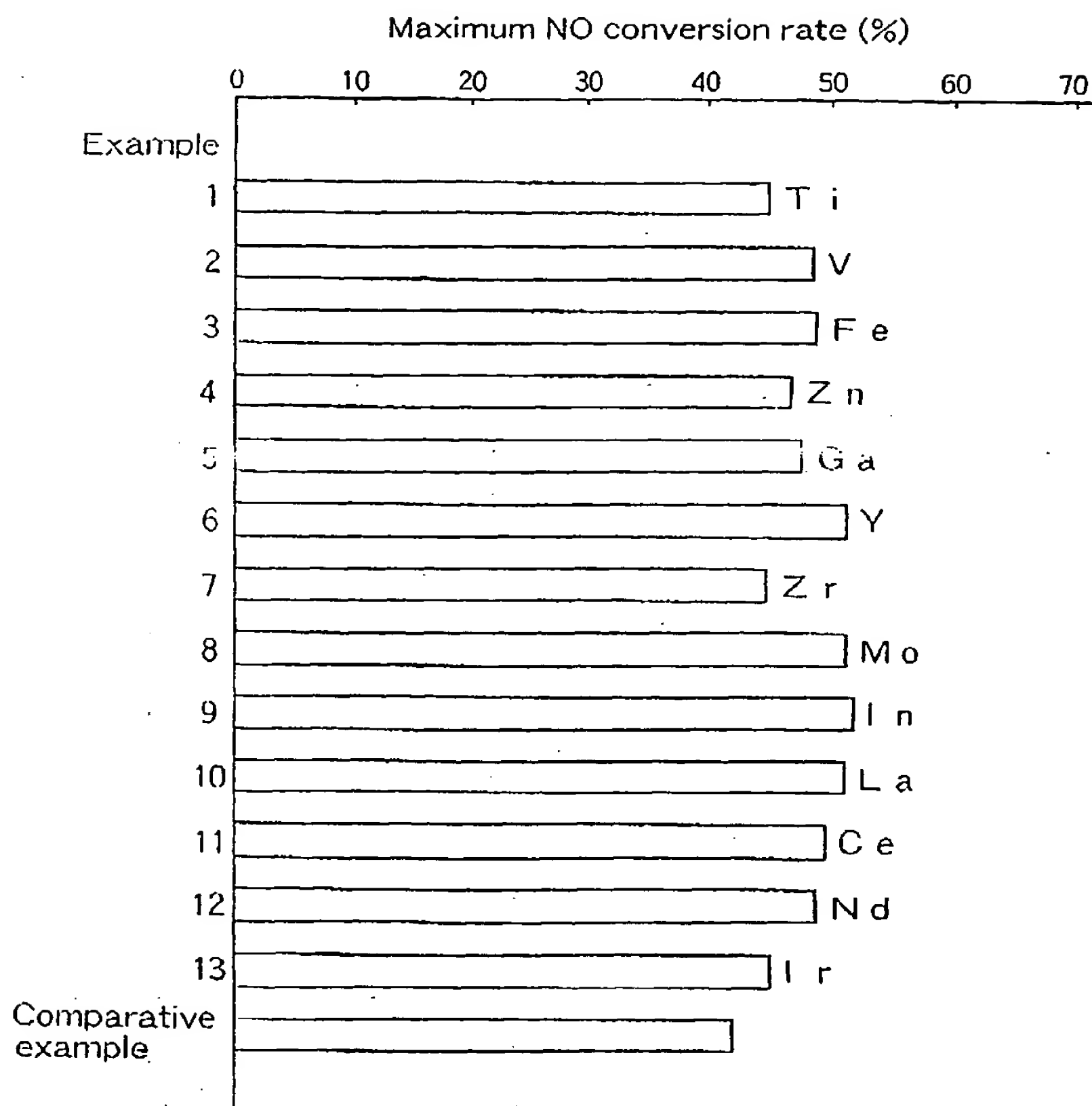


FIG. 5

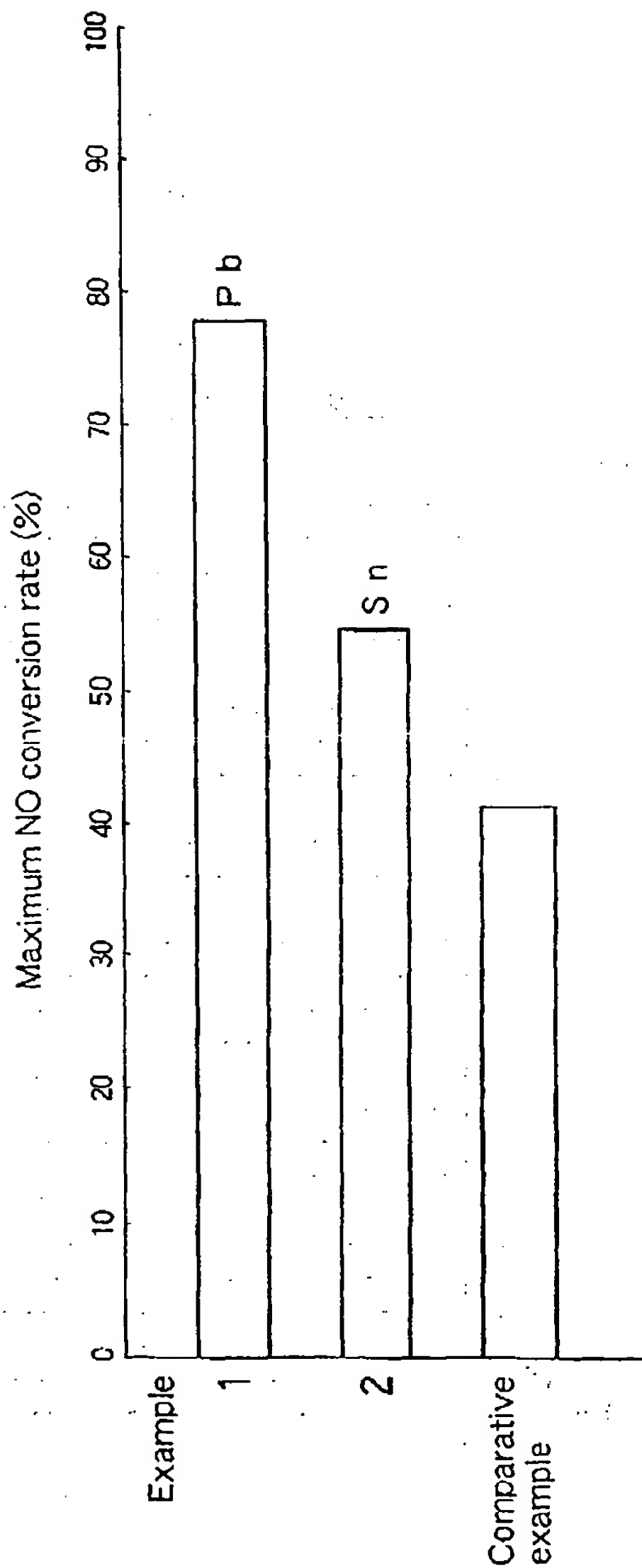
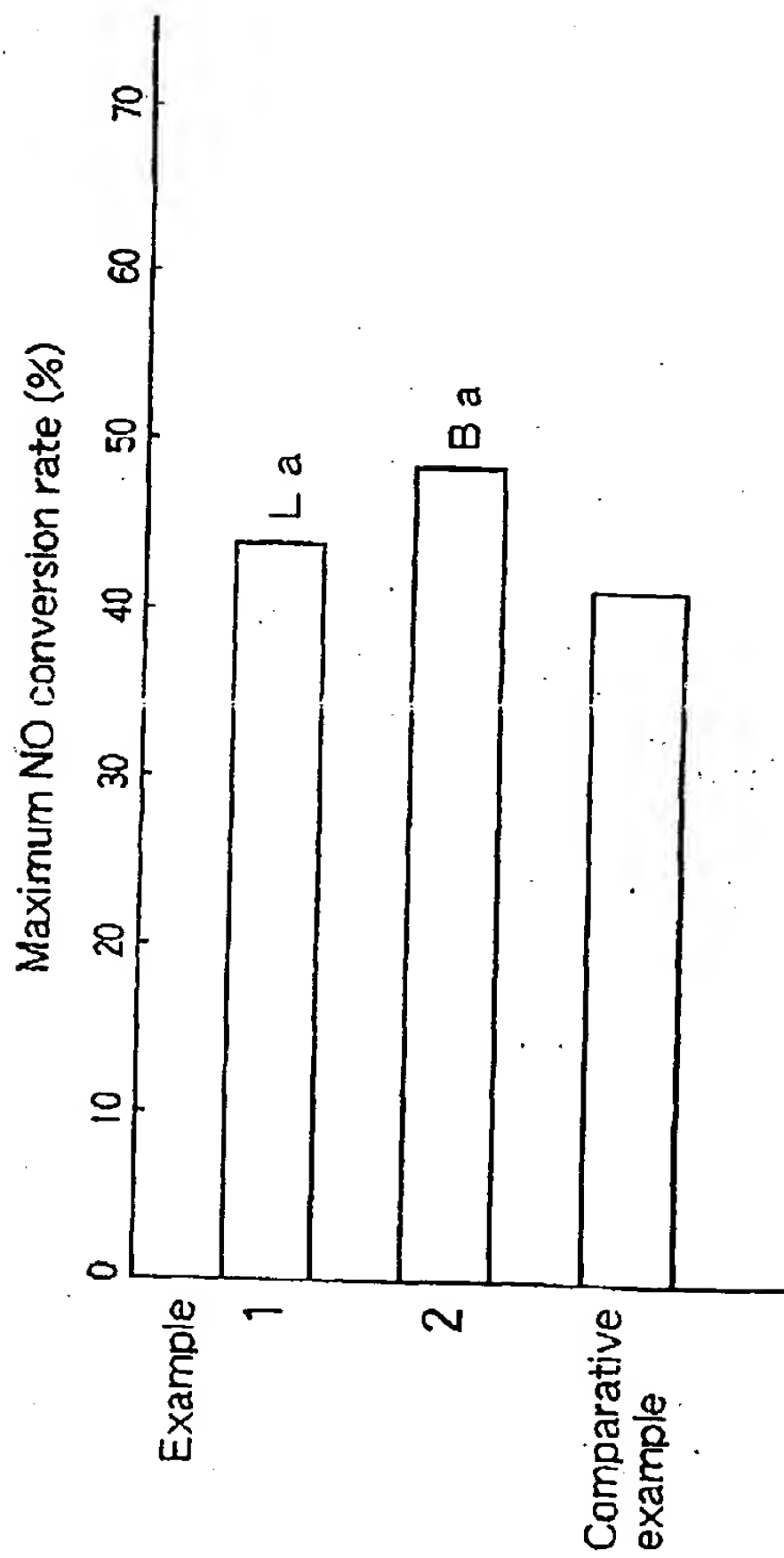


FIG. 6







European Patent  
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## EUROPEAN SEARCH REPORT

Application Number  
EP 97 30 2700

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Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. CL.6)
X	EP 0 671 208 A (HONDA MOTOR CO LTD) 13 September 1995 * page 4, line 34 - line 38 * * page 6, line 50 - page 7, column 38; claims 6-17; examples *	1-6	B01D53/94 B01J29/06 B01J23/10 B01J23/63
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Y	EP 0 613 714 A (TOYOTA MOTOR CO LTD ; TOYODA CHUO KENKYUSHO KK (JP); CATALER IND CO) 7 September 1994 * page 5, line 35 - line 44; tables 6,7 *	1-6	
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The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 18 July 1997	Examiner Eijkenboom, A
CATEGORY OF CITED DOCUMENTS X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background (I) : non-written disclosure P : intermediate document T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document			

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